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⑦① Applicant: **E.I. DU PONT DE NEMOURS AND COMPANY,**
Legal Department 1007 Market Street, Wilmington
Delaware 19898 (US)

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⑦② Inventor: **Coughlin, James Edward, 2051 East Albright**
Street, Philadelphia Pennsylvania 19134 (US)
Inventor: **Sommerveld, Eugene Gary, 28 Farnwood Road,**
Mt. Laurel New Jersey 08054 (US)
Inventor: **Strolle, Clifford Hugh, 531 Barry Drive,**
Springfield Pennsylvania 19064 (US)

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⑦④ Representative: **Jones, Alan John et al, CARPMAELS &**
RANSFORD 43 Bloomsbury Square, London, WC1A 2RA
(GB)

⑤④ **Ternary adhesive systems.**

⑤⑦ Disclosed are adhesive systems and adhesives formed from (A) hydroxyl-terminated, preferably branched, polyols, (B) isocyanate-capped, polyol-based urethanes and (C) polyisocyanate crosslinking agents. In their preferred embodiments, they are applicable by direct gravure procedures and are useful in boil-in-bag technology.

TITLE

Ternary Adhesive Systems

BACKGROUND OF THE INVENTION1. Field of the Invention

5 This invention relates to ternary adhesives and systems formed from a branched polyester and two isocyanates, an isocyanate-capped polyester-urethane and a polyisocyanate. All of these are very soluble in organic solvents and can comply with pollution-abatement regula-
10 tions. The adhesives contain aromatic groups and are particularly useful in bonding poly(ethylene terephthalate) to other flexible plastic substrates.

2. Prior Art

 Bock et al. U.S. Pat. 3,584,075 shows a poly-
15 urethane adhesive based on an aliphatic polyester, an aromatic polyester, and a diisocyanate.

 Schloss U.S. Pat. 3,666,835 shows textile laminating adhesives based on a hydroxyl-terminated urethane prepolymer and an isocyanate-terminated urethane
20 prepolymer.

 Fryd U.S. Pat.'s 3,763,079 and 3,804,810 show hydroxyl-terminated polyurethanes formed from copolyesters.

 Yamazaki et al. U.S. Pat. 4,206,299 shows an adhesive for plastics and metal foil containing a silane
25 coupling agent and acknowledges certain other prior art.

 Sommerfeld et al. U.S. Pat. 4,298,724 (Sommerfeld) shows branched polyesters some of which are useful in this invention and procedures for making them applicable to all.

30 The above-identified art is incorporated herein by reference.

SUMMARY OF THE INVENTION

 The present invention comprises novel laminating adhesive compositions formed at the time
35 of use by the interaction of three precursors, namely:

- A. a hydroxyl-terminated branched polymer of low-molecular weight, preferably a branched polyester;
B. an isocyanate-terminated substantially linear urethane of low molecular weight, preferably a polyester-urethane; and
5 C. a polyisocyanate crosslinking agent.

The compounds of B are themselves novel non-volatile isocyanates. Therefore, they form one aspect of the invention. Furthermore, since B and C are both
10 isocyanates, they can be premixed and packaged together if it is so desired. The isocyanate mixture or blend constitutes an aspect of the invention. The laminate products are another aspect of the invention.

When all three of the listed components are
15 mixed, they form a high solids adhesive with little polluting solvent and many remain stable at room temperature (ca. 25°C) long enough (for up to 8 hours) to be used, for example, in direct gravure application on a conventional coater/laminator with sufficient green strength (adhesion before final curing) for post handling. The preferred cured adhesive is both sufficiently adherent and
20 sufficiently heat resistant to serve as a boil-in-bag adhesive.

Details of the invention follow.

25 THE HYDROXYL-TERMINATED BRANCHED POLYESTER

A. The first of the three precursors of the present adhesives, polymer A, is a polymeric polyol, preferably a branched hydroxyl-terminated polyester. The polyester is prepared in a single step by conventional
30 methods for preparing polyesters from conventional materials, e.g., (1) a diol, (2) generally a higher polyol (i.e., one containing more than two hydroxyl groups per molecule), (3) a dibasic aromatic acid, and
35 (4) a dibasic aliphatic acid.

Diols (1) usable here are any of those commonly employed. They can be aliphatic or aromatic and generally

have 2-14 carbons. They can be substituted with or interrupted with noninterfering groups such as O, S, halogen and the like. Suitable diols include: ethylene glycol, propylene-1,2-glycol, propylene-1,3-glycol, butylene-1,3-
5 diol, butylene-1,4-diol, butylene-2,3-diol, neopentyl-glycol, i.e., 2,2-dimethylpropane-1,3-diol, 2,2-diethylpropane-1,3-diol, 2-methyl-2-propylpropane-1,3-diol, decamethylene glycol, dodecamethylene glycol, thioethylene glycol, monoethyl ether of glycerine, α - and β -
10 allyl ethers of glycerol, and the like. Polycaprolactone diol, the reaction product of caprolactone and ethylene glycol, can also be used.

Preferably the diols will have about 2-8 carbon atoms; most preferably they will have about 2-6 carbon
15 atoms. Ethylene glycol is particularly preferred.

Higher polyols (2) used as branching agents, preferably have 3-14 carbons and a functionality greater than 2. They include triols, tetraols, etc., such as glycerine, trimethylolpropane, pentaerythritol,
20 1,2,6-hexanetriol, and the like.

Aromatic (3) and aliphatic (4) acids can be unsubstituted or can contain, be substituted with or be interrupted by noninterfering groups such as O, S, halogen, keto and the like. Suitable dicarboxylic acids include: malonic, succinic, glutaric, adipic, pimelic,
25 suberic, azelaic, sebacic, brassylic, maleic, fumaric, dilinoleic, diphenic, phthalic, tetrachlorophthalic, isophthalic, terephthalic, orthophthalic, cyclohexane dicarboxylic, p-phenylene diacetic, naphthalene dicarboxylic, dihydromuconic, β -methyl adipic, trimethyl
30 adipic, ethylether-2,2'-dicarboxylic, and the like. Anhydrides of these dicarboxylic acids can be used where they exist. Lower alkyl esters of these acids can also be used in a transesterification process.

Preferably, the dicarboxylic acids, anhydrides or esters of dicarboxylic acids will have about 4-12 carbon atoms, and include terephthalic acid, isophthalic acid, orthophthalic acid, azelaic acid, adipic acid, and a mixture of C₄-C₆ aliphatic dicarboxylic acids.

The usable polyesters are generally prepared from the ingredients of the products of the above-mentioned Sommerfeld application and in substantially the same manner. They are not, however, coextensive with those products since some of the unsatisfactory oils of that application can be employed here. This fact is evident from the ratios of materials used.

The first of these ratios is X_{1A} , where

$$X_{1A} = \frac{\text{Total Moles of Polyol.}}{\text{Total Moles of Diacid}}$$

In a broad range, X_{1A} extends between 1.05 and 1.5. More narrowly, in a preferred range, it is between 1.2 and 1.3. X_{1A} defines the molecular weight (\bar{M}_n) of the pre-polymer, i.e., $\bar{M}_n = 1,000-5,000$. (In all the ratios used, the denominator is assumed as 1 unless given.)

A second ratio is X_{2A} , where

$$X_{2A} = \frac{\text{Total Moles of Diol}}{\text{Total Moles of Higher Polyol}}$$

Broadly, X_{2A} is between ∞ and 0.86, preferably between ∞ and 2.25, i.e., higher polyol can be omitted. More preferably, however, it is between 1.2 and 3.3. X_{2A} defines the branching of the polyester.

A third ratio is:

$$X_{3A} = \frac{\text{Moles of Aromatic Acid}}{\text{Moles of Total Acid}}$$

The presence of some aromatic material is important in this invention, e.g., to increase adhesion, heat resistance, etc., of the product. It can be supplied from two sources, from the polyester A and the polyester-urethane B. Consequently, X_{3A} lies in the range 0-ca.

0.8, 0, of course, indicating that aromaticity is supplied by component B. Preferably, however, the lower limit for X_{3A} should be about 0.3 and a preferred range is 0.3-0.65.

5 As indicated in the Sommerfeld patent, the polyesters A can be prepared very simply. The ingredients may be mixed in proportions indicated by the ratios X_{1A} , X_{2A} , and X_{3A} and heated in the range of about 160-260°C with removal of water as the reaction
10 proceeds. The product has an acid number of less than 5 or, often, less than 1. Alternatively, transesterification can be employed using lower alkyl esters such as methyl esters rather than acids. In this alternate process, a transesterification catalyst such as an organo-
15 ometallic compound of tin, etc., is needed and an alcohol rather than water is removed. \bar{M}_n by either route is about 1,000-5,000.

THE ISOCYANATE-TERMINATED URETHANE

The polyester-urethane B is an isocyanate-
20 terminated polymer of low-molecular weight formed by chain extending and endcapping at least one substantially linear hydroxyl-terminated polyester, here regarded as a pre-polymer, by reaction with at least one diisocyanate. The reaction including ingredients and conditions but
25 usually without catalyst is otherwise substantially as shown by the Fryd patents (see especially columns 1-4 of 3,763,079) and proceeds by steps. The polyester pre-polymer is first formed by direct action between diol
30 and diacid. It is then reacted with a diisocyanate possibly in the vessel in which it was prepared. Copolyesters are not essential, however, only preferred, and two different dicarboxylic acids are not essential.

Ratios can be set up for B as for A, above.

Thus, for the prepolymer and hence for B itself,

$$X_{1B} = \frac{\text{Total Moles of Polyol}}{\text{Total Moles of Diacid}}$$

is within the range 1.05-1.5 ($\bar{M}_n = 500-4,000$).

5
$$X_{2B} = \frac{\text{Total Moles of Diol}}{\text{Total Moles of Higher Polyol}}$$

is within the range 5- ∞ , since some branching is satisfactory. Preferably, X_{2B} is at least 10. And

$$X_{3B} = \frac{\text{Moles of Aromatic Acid}}{\text{Total Moles of Acid}} = 0-0.8.$$

10 Since isocyanate-terminated or end-capped products are desired here, the ratio of isocyanate to hydroxyl is appreciably larger than in Fryd who teaches non-NCO-containing polyester-urethanes. This additional equivalent ratio,

15
$$X_{4B} = -\text{NCO}/-\text{OH},$$

is broadly in the range 2-1.2 with the range 1.7-1.3 being preferred.

The (co)polyesters are produced by conventional techniques which are well known. Ordinarily, the reactants will be admixed in a suitable reaction vessel, with heating to a temperature of about 150°C-250°C for 5-15 hours to produce the polyester. Diols, dicarboxylic acids and higher polyols, where employed, can be those given above for the preparation of polyester A. A preferred polyol branching agent is trimethylol propane.

The polyester-urethanes of the invention are obtained by reacting directly the substantially linear hydroxyl-terminated polyester prepolymers with diisocyanates, generally in an organic solvent. Any of the common organic solvents are usable so long as they are dry and lack hydroxyl or other groups reactive with isocyanate. Ketones such as acetone, methyl ethyl ketone and the like are particularly useful. In this reaction, the equivalent ratio of isocyanate from the diisocyanate to



hydroxyl from the prepolymer are greater than 1/1 as is evident from the values of X_{4B} , above.

The diisocyanates for use with the polyesters in this invention can be aliphatic or aromatic. Suitable isocyanates include: hexane-1,6-diisocyanate, decane-1, 10-diisocyanate, diisocyanates derived from dimerized fatty acids, phenylene-1,4-diisocyanate, toluene-2,4-diisocyanate, toluene 2,6-diisocyanate, naphthylene-1, 5-diisocyanate, diphenylmethane-4,4'-diisocyanate, diphenylmethane-3,3'-dimethoxy-4,4'-diisocyanate, dicyclohexylmethane-4,4'-diisocyanate, etc.

Preferred are toluene-2,4-diisocyanate, toluene-2,6-diisocyanate and mixtures thereof.

The products B of the polyester-isocyanate reaction are very soluble but nonvolatile isocyanates and have the general utilities of isocyanates, e.g., as reactants with hydroxyl-carrying compounds to prepare polyurethane coating materials, or the like. In some cases, they can serve as crosslinkers (see Example 15, below), but here the use of a polyisocyanate C is preferred.

THE POLYISOCYANATE

The precursors A and B are reacted in situ in the laminate of the invention to form what is basically a block copolymer. This procedure permits low molecular weight and low viscosity of the components in the adhesive of the mix directly after combining the components but develops a high molecular weight product by extension in situ upon the workpiece, i.e., a substrate such as film, metal, etc., upon curing. Sufficient crosslinking between the hydroxyl Groups of A and the isocyanate groups of B is not generally attainable without the presence of a more highly functional crosslinking agent. To achieve the desired results, polyester A is used in excess over polyester-urethane B, and some of the isocyanate deficiency is supplied by at least one polyisocyanate crosslinking agent C having an average functionality greater than 2.



Usable polyisocyanates include aliphatic or aromatic compounds such as 4,4',4"-triisocyanatotriphenyl methane, 1,3,5-triisocyanatobenzene, 2,4,6-triisocyanatotoluene, and the like, biurets of the diisocyanates mentioned above such as the trimerization product of hexane-1,6-diisocyanate, adducts of one or more diisocyanates with one or more higher polyols such as propane triol, 1,2,6-hexane triol, trimethylolpropane, pentaerythritol, etc. Preferred polyisocyanates are the adducts of aromatic diisocyanates with trimethylolpropane in a 3/2 or 5/2 mole ratio to yield a polyisocyanate having a functionality of 3 or 4, such as the adduct of toluene-2,4-diisocyanate or toluene-2,6-diisocyanate, or mixtures thereof, with trimethylolpropane in a 5/2 mole ratio.

The proportions of B and C in the mixture employed can vary within limits but at least 50% (by weight) of B is preferred. A broad range of B is 94-50% with a preferred range of 90-70%. Conversely, the ranges of C are 6-50 and 10-30%, respectively. The higher ranges of C, e.g., above about 30%, result in embrittlement but can be used where brittle adhesives are desired. All of these compounds are very soluble in nonreactive organic solvents, e.g., ketones such as methyl ethyl ketone (MEK), esters such as ethyl acetate (EA), etc. Consequently, solutions of 50-70% by weight at room temperature can readily be obtained, with above 60%, i.e., 62-75%, being generally made. These solutions or blends have the normal utilities of polyfunctional isocyanates.

The ratio of polyester A to the combined isocyanates is also of importance. A should form 25-75% by weight of the final adhesive mixture and combined B and C should form the remaining 75-25%, all based on the solids present. For higher solids use, A should form

40-65% of the final adhesives. The total aromaticity derived from the aromatic acids in A plus B should be no less than 15% on a mole basis of the total acids present.

5 The two isocyanates used in the adhesive, polyester-urethane B and polyisocyanate C, may conveniently be mixed before the reaction with polymer A. They may, in fact, be packaged together and used as one package of a two-package adhesive system. Solvents are
10 generally used to lower the viscosity sufficiently to permit utilization while maintaining EPA compliance in the final blend. Any organic solvent inert to organic isocyanates can be employed, the amount being varied in accord with the application requirements. Representa-
15 tive solvents include methyl ethyl ketone, methyl isobutyl ketone, acetone, dimethyl sulfoxide, isophorone, mono(lower-alkyl) ethers of ethylene glycol acetate, mono(lower-alkyl) ethers of diethylene glycol acetate, lower alkyl acetates, etc.

20 A catalyst to speed up reaction between polyester A of the first package and isocyanates B and C of the second package may be added to either package, if desired. The catalyst, useful particularly at lower temperatures, can consist of organometallics such as
25 dibutyltin dilaurate, etc., organic bases such as amines, and the like. Up to about 100 ppm based on total package solids is effective. Catalyst can also be added separately to the adhesive when it is mixed, if desired.

THE ADHESIVE

30 Polyester A and the two isocyanates B and C (separately or packaged) are mixed together at the time of use. Because of their solubility and low viscosity in organic solvents, they produce high solids adhesives, i.e., adhesives containing 50-90% by weight of solids or here preferably
35 60-75% or most preferably 65-70%, and are useful in



minimizing pollution. They can be employed with a wide variety of substrates, e.g., paper, plastic film, glass, wood, and the like.

The mixed adhesives can be applied to sub-
5 strates in any convenient manner. If, however, their viscosity is less than 1000 centipoise at room temperature (about 20°C), they can be applied by direct gravure procedures. The present adhesives in general have such a viscosity, i.e., less than 1000 cps, and can retain it for up to
10 8 hours. Thus, they can be used with conventional direct gravure machinery, e.g., the Faustel Model TT coater/laminator made by Faustel, Inc., Butler, Wisconsin, currently employed with conventional, i.e., not high solids, adhesives. Expensive conversion to offset gravure
15 machinery is thus avoided. As far as is known, these novel ternary adhesives are the first high solids adhesives applicable by direct gravure to give the balance of properties heretofore mentioned.

In their preferred embodiment, the final prod-
20 ucts of the invention possess sufficient green strength and sufficient resistance to heat, moisture, oils and acid to be used as boil-in-bag adhesives. Their aromatic content makes them especially valuable in bonding flexible films, e.g., polyethylene, metal foil, etc., to
25 poly(ethylene terephthalate).

In usual boil-in-bag technology, poly(ethylene terephthalate) and polyethylene films are bonded together by means of adhesive (preferably by direct gravure), the resultant laminated film is folded, and the
30 (inner) polyethylene film is itself sealed by heat around two edges to form the inside of a pouch. Food is placed in the pouch and the polyethylene film is heat sealed to itself along the third edge (the fourth "edge" is the fold). The sealed pouch is placed in boiling
35 water for one hour. If no delamination occurs within this period, the sealed bag is considered acceptable.

EXAMPLES

There follow some examples illustrating the invention. A, B and C represent respectively and as above the hydroxyl-terminated branched polyester, the isocyanate-terminated polyester-urethane and the poly-isocyanate crosslinking agent. The last mentioned was, in all cases, Mondur® CB-75, the 5/2 molar product of toluene diisocyanate (TDI) and trimethylol propane supplied at 75% solids in ethyl acetate (EA) by Mobay Chemical Company. Temperatures are in degrees centigrade and percentages and proportions in terms of weight unless otherwise noted.

Example 1 represents the preferred embodiment of the invention. It also shows the procedure used in all examples but no order of preparation of the examples is intended by the order of listing.

EXAMPLE 1

(a) A 12-1,3-necked resin flask fitted with a fractionating column mounted with a water-separator or variable take-off head, an agitator and a thermometer was charged with:

<u>Ingredient</u>	<u>Weight (g)</u>
Trimethylol propane (TMP)	970.48
Ethylene glycol (EG)	2244.33
25 Terephthalic acid (T)	901.06
Isophthalic acid (I)	1502.00
Azelaic acid (9)	4087.69
	9701.56

The reaction mixture was heated to 260° as 1301.69g of water was collected over a 12-hr. period. The vapor temperature was held below 105°C. At Acid No = 0.94, the charge was cooled and thinned with methyl ethyl ketone (MEK) to 85% solids. The product was a solution of the polyester TMP/EG//T/I/9 of the mole ratio 0.2/1.0//0.15/0.25/0.60: Gardner Holdt visc = X (1290 cps);

Hydroxyl No = 144 (Theo = 145); Residual EG = 0.43%;
 Res TMP = 0.01%; % H₂O = 0.043%; GPC \bar{M}_n = 2900, \bar{M}_w =
 9100, \bar{M}_z = 23,000; D = 3.2; sp g dist = 1.002.

- (b) 1. A polyester prepolymer was prepared in
 5 a flask as above charged with:

Ingredient	Weight (g)
EG	3,636.65
T	2,471.16
I	1,272.76
10 9	4,241.76
	11,622.50

The reaction mixture was heated to 260° as 1,623g of
 water was collected over a period of 13 hrs.. The mix-
 15 ture was cooled at a final Acid No of 4.5 to give a
 prepolymer of the mole ratio EG/T/I/9 1.3//0.33/0.17/-
 0.50; Hydroxyl No = 144 (Theo = 152); Resid EG = 0.77%;
 visc = 800 p; H₂O = 0.75%; GPC \bar{M}_n = 1500, \bar{M}_w = 2400,
 \bar{M}_z = 3600; D = 1.6g; sp g dist = 1.002.

2. Polyester prepolymer from 1, above, was
 20 end-capped and chain-extended with toluene diisocyanate
 (TDI) in the equivalent ratio X_{4B} = 1.67 (based
 on Hydroxyl No 130). A 3-necked flask fitted with a
 reflux condensor, and agitator was charged with 1500 g
 25 of the polyester prepolymer and 668.3 g of ethyl acetate.
 The mixture was agitated, purged and blanketed with
 N₂ and heated to 60° at which time 505 g of TDI was added
 as rapidly as possible. The reaction exotherms
 to 70-75° and heat was applied to bring the reaction mass
 30 to reflux at 86-88°. The reaction was held for 6 hrs. at
 reflux and cooled to room temperature to give a solution:
 Gardner-Holdt visc = Z 2-1/4 (3340 cps) at 75% solids
 (G-H visc = H (200 cps) at 60% solids); -NCO = 3.68% (on
 solids); Resid TDI = 0.30%; GPC \bar{M}_n = 3900, \bar{M}_w = 7800,
 35 \bar{M}_z = 1400.

(c) Polyester A and the isocyanate-terminated polyester-urethane B, both above, and polyisocyanate C (Mondur® CB-75) were blended together in MEK for one-half hour at the time of use to contain:

5	<u>Component</u>	<u>Weight of Charge (g)</u>
	A (85% solids in MEK)	67.3
	B (75% solids in EA)	44.9
	C (75% solids in EA)	12.1
	MEK	29.5
10		153.8

The weight ratio A/B/C = 57.24/33.67/9.09 (dry); B/C = 78.74/21.26 (dry); Solids = 65%; visc = 15-25 sec Zahn No. 3 (120-300 cps).

The mixture thus prepared was coated within 8 hours onto 48 LB Mylar® (trademark of E. I. du Pont de Nemours and Company) poly(ethylene terephthalate) film and laminated in rolls by direct gravure to medium density polyethylene (MDPE) film by means of a Faustel Model TT coater/laminator (Faustel, Inc., Butler, Wisconsin). The following conditions were maintained throughout the test:

	Cylinder	200 TH (trihelical)
	Oven Temp	93°
	Speed	30 ft/min (9.1 m/min)
25	Coater Nip	80 psi (5.6 Kg/cm ²).

Coating weights were determined to be 1.1 to 1.6 lbs/300 ft² (1.7-2.6g/m²). Peel strengths (90° and 180°, angular) were determined using an Instron "C" cell at 25° with a crosshead speed of 12 in/min (30 cm/min). Green strength values (taken within 2 hours) were in the range 100-300 g. After three days, bond strengths were in the range 600-1300 g. Generally, one of the substrate films then tore before the bond. Similar results were obtained after 8 weeks.

(d) Pouches (6" x 6"; 15 cm x 15 cm) were prepared from the Mylar®/MDPE laminate from (c) by folding and sealing on a Sentinel Heat Sealer (375°F; 40 psi; 1.0 sec; 190°C; 2.8 Kg/cm²; 1.0 sec) along three edges of the polyethylene inner layer to form bags open at one edge. Two separate bags were filled 2/3 full of water and a commercial tomato sauce respectively. The thus-filled bags were heat sealed on the open edge after air was manually squeezed from them. The bags were then held for an hour in boiling water. The bags were regarded as satisfactory, i.e., no delamination occurred, after the treatment described.

Examples 2 and 3

Example 1 was substantially repeated except that the hydroxyl-terminated branched polyester A was different and the ratios of A, B and C were varied. The isocyanate-terminated polyester-urethane was as prepared in Example 1(b) and the polyisocyanate was Mondur® CB-75. The same ingredients were used in the polyester A of Examples 2 and 3 as in Example 1 but the TMP/EG//T/I/9 mole ratio was 0.3/1.0//0.2/0.3/0.5.

The adhesive was blended as follows:

<u>Component</u>	<u>Example 2</u> <u>(g)</u>	<u>Example 3</u> <u>(g)</u>
A (85% solids in MEK)	962.8	665.0
B (75% solids in EA)	641.9	665.0
C (75% solids in EA)	173.3	142.0
MEK	422.0	328.0

For Example 2, the dry Weight Ratio A/B/C was 57.24/33.67/9.09 and the B/C Ratio was 78.74/21.26.

Product (65% solids in solvent) showed: visc = 23 sec (220 cps). For Example 3, the dry Weight Ratio A/B/C was 48.29/42.61/9.1 and the B/C Ratio was 82.4/17.60.

Both of these products were excellent adhesives with good boil-in-bag properties when applied by direct gravure as in Example 1.

Example 4

Example 1 was substantially repeated with the variation of slight branching in the polyester prepolymer from which Component B, the polyester-urethane, was prepared. The Components A and C were the same as in Example 1.

For the polyester prepolymer, a 5-l, 3-necked flask fitted with a fractionating column mounted with a water separator or variable take-off head, agitator, and thermometer was charged with:

	<u>Ingredient</u>	<u>Weight (g)</u>
	TMP	92.8
	EG	515.2
	T	172.4
15	I	287.4
	9	781.3

This charge corresponds to the mole ratio TMP/EG//T/I/9 of 0.1/1.2//0.15/0.25/0.6 and a "branching" ratio X_{2B} of 12. The charge was heated to 260° as 249 g of water was collected over a 7-hour period, the vapor temperature being held below 105°. At Acid No = 0.02, distillation was stopped and the batch cooled in preparation for the extension reaction. For the prepolymer: GPC \bar{M}_n = 1800, \bar{M}_w = 3600, and \bar{M}_z = 6400; Hydroxyl No = 149 (Theo = 170); H_2O = 0.37%; sp g dist = 1.002.

The branched prepolymer was chain-extended and end-capped with TDI in the -NCO/-OH Equivalent Ratio X_{4B} = 1.7/1 (based on Hydroxyl No = 165). Prepolymer (1500 g) and 717 g of EA were charged into a 3-necked flask equipped as in Ex. 1(b) (2). The mixture was agitated, purged and blanketed with N_2 and heated to 50°. TDI (295 g) was added at 50° as rapidly as possible resulting in an exotherm to 60-65°. Heat was applied to bring the reaction mass to reflux (88°) and the reaction was held for 6 hours at reflux. When cooled, the product solution showed: Gardner-Holdt visc = Z-2 (3260 cps) at 75%

solids (G-H visc = J (250 cp) at 60% solids); -NCO = 5.24% (on solids); Resid TDI = 0.64% (on total); GPC \bar{M}_n = 4000, \bar{M}_w = 15,000, \bar{M}_z = 41,000.

An adhesive was made up as follows:

Ingredient	Weight (g)
A (from Ex. 1; 85% solids in MEK)	758.6
B (branched as above; 75% solids in EA)	505.7
C (Mondur® CB-75; 75% solids in EA)	210.4
MEK	325.3

The weight ratio A/B/C = 54.56/32.09/13.35 (dry); B/C = 70.62/29.38 (dry); Solids = 65% (total solids); visc = 22 sec Zahn No. 3 (ca 200 cps).

When the adhesive system thus blended was applied to polyethylene/poly(ethylene terephthalate) film by direct gravure as in Example 1, the laminate showed excellent green strength and, upon curing, excellent boil-in-bag properties.

Examples 5 to 14

The following Examples in Table I represent a number of polyester compositional variables. Various weight ratios of Components A/B/C and Components B/C are demonstrated. In all cases, A/B/C and B/C are on a dry weight basis. All Examples were evaluated at 65 wt. % solids.

Table I

Component A		Table 1										
Ex.	Composition ¹	Mole Ratio		X _{1A}	X _{2A}	X _{3A}						
5	EG//T/I/9	1:06//.33/.17/.50		1.06	∞	0.5						
	6 TMP/EG//T/I/9	.2/1.1//.2/.3/.50		1.30	5.5	0.5						
	7 TMP/EG//T/I/9	.1/1.2//.15/.25/.60		1.30	12.0	0.4						
	8 TMP/EG//T/I/9	.2/1.1//.15/.25/.60		1.30	5.5	0.4						
	9 EG/NPG//T/I/9/6 ⁸	1.0/0.3//.15/.25/.3/.3		1.30	∞	0.4						
	10 TMP/EG//T/I/9	.3/1.0//.2/.3/.5		1.30	3.33	0.5						
10	11 TMP/EG//T/I/9	.3/1.0//.2/.3/.5		1.30	3.33	0.5						
	12 TMP/NPG/EG//T/I/9/6	.2/.3/.7//.15/.25/.3/.3		1.20	5.0	0.4						
	13 TMP/NPG/EG//T/I/9	.2/.3/.7//.15/.25/.60		1.20	5.0	0.4						
	14 TMP/NPG//T/I/9	.2/1.0//.15/.25/.60		1.20	5.0	0.4						
	15 TMP/EG//T/L/9	.2/1.1//.2/.3/.50		1.30	5.5	0.5						
15							Remarks ²					
							Re-					
							tained					
							Direct					
							Gravure ⁶					
	Ex.	A	B	C ⁷	B	C ⁷	VISC (CPS)	BIB ³	Green Str. ⁴	Bond Str. ⁵	Direct Gravure ⁶	
	5	49.0	43.30	7.70	84.90	15.10	1300	Yes	Yes	Yes	No	
	6	28.05	62.86	9.09	87.40	12.60	1000	Yes	Yes	Yes	No	
20	7	48.29	42.61	9.10	82.40	17.60	175	Yes	Yes	Yes	Yes	
	8	48.29	42.61	9.10	82.40	17.60	160	Yes	Yes	Yes	Yes	
	9	48.29	42.61	9.10	82.40	17.60	190	No	Yes	Yes	Yes	
	10	59.95	35.27	4.78	88.06	11.94	220	No	Yes	Yes	Yes	
25	11	52.46	30.85	16.69	64.89	35.11	230	Yes	Yes	No	Yes	
	12	54.20	36.10	9.70	78.82	21.18	300	No	Yes	Yes	Yes	
	13	54.20	36.10	9.70	78.82	21.18	300	No	Yes	Yes	Yes	
	14	54.20	36.10	9.70	78.82	21.18	300	No	Yes	Yes	Yes	
	15	30.85	69.15	0.0	100.0	0.0	1000	No	Yes	Yes	No	
30	1. Composition B: in all Examples except Ex. 5, Polyester B = EG//T/I/9, 1.3//0.33/0.17/0.50; for Ex. 5, EG//T/I/9, 1.06//0.33/0.17/0.50. X _{2B} = ∞ in all cases, X _{3B} = 0.5 in all cases, X _{4B} = -NCO/-OH equivalent ratio = 1.67 in all cases.											
	2. All show adhesive utility in various end uses.											
	3. BIB = Boil-in-bag test.											
	4. Green Str.=Initial adhesive strength up to 2 hrs. after application											
	5. Retained Bond Str.=Aged adhesive strength up to 2 mos.											
35	6. Direct Gravure=May be applied @ 65-70 wt. % solids. Those Exs. labeled "No" are applicable by other methods, e.g., offset gravure.											
	7. Composition C = Mondur® CB-75 in all cases.											
	8. NPG = Neopentyl glycol; 6 = Adipic acid.											

CLAIMS:

1. A ternary adhesive system consisting essentially of:

- A. at least one hydroxyl-terminated
 5 polymeric polyol having a molecular weight \bar{M}_n of about 1,000-5,000 and soluble in methyl ethyl ketone or ethyl acetate to the extent of at least 65% by weight;
- B. an isocyanate-capped polyol-urethane
 10 formed from at least one polyol having a molecular weight \bar{M}_n of about 500-4,000 which has been extended and capped with a diisocyanate in the -NCO/-OH ratio of 2/1-1.3/1 and is capable of forming a block copolymer with and thereby extending polyol A; and
- 15 C. a polyisocyanate crosslinking agent
 C supplying 6-50% by weight in a mixture of B plus C.

2. An adhesive system of Claim 1 wherein A forms 25-75% by weight of the solids present therein.

20 3. An adhesive system of Claim 1/^{or Claim 2} wherein the polyol of A and the polyol of B are polyesters.
 any one of 1 to

4. An adhesive system of/~~Claims~~ 3 wherein the hydroxyl-terminated polyester A is a copolymer of at least one aromatic dicarboxylic acid and at
 25 least one aliphatic dicarboxylic acid with at least one polyol,

the ratio $X_{1A} = \frac{\text{Total Moles of Polyol}}{\text{Total Moles of Diacid}}$
 extending between 1.05/1 and 1.5/1,

30 the ratio $X_{2A} = \frac{\text{Total Moles of Diol}}{\text{Total Moles of Higher Polyol}}$
 extending between ∞ and 0.86/1, and

the ratio $X_{3A} = \frac{\text{Moles of Aromatic Acid}}{\text{Moles of Total Acid}}$
 extending between 0 and about 0.8/1.

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5. An adhesive system of/Claims 1/wherein the polyester-urethane B is formed from a hydroxyl-bearing polyester made from at least one polyol and at least one diacid wherein

5 the ratio $X_{1B} = \frac{\text{Total Moles of Polyol}}{\text{Total Moles of Diacid}}$ is within the range 1.05/1-1.5/1 and the molecular weight $\bar{M}_n = 500-4,000$,

10 the ratio $X_{2B} = \frac{\text{Total Moles of Diol}}{\text{Total Moles of Polyol}}$ is within the range 5/1- ∞ ,

the ratio $X_{3B} = \frac{\text{Moles of Aromatic Acid}}{\text{Total Moles of Acid}}$ is within the range 0-0.8/1, and

15 the ratio $X_{4B} = \frac{\text{Equivalents of -NCO}}{\text{Equivalents of -OH}}$ is within the range 2/1-1.3/1.

6. A substantially linear isocyanate-capped polyol-urethane formed from a polyol having a molecular weight \bar{M}_n of about 500-4,000 which has been extended and capped with a diisocyanate in the -NCO/-OH ratio of 2/1-1.3/1 and which is capable of forming a block copolymer with a hydroxyl-terminated polyol.

7. A high-solids adhesive formed in situ wherein a polymeric polyol A having a molecular weight \bar{M}_n of about 1,000-5,000 and soluble in methyl ethyl ketone or ethyl acetate to the extent of at least 65% by weight is chain-extended and thereby increased in molecular weight by reaction with an isocyanate-capped polyester-urethane B making a block copolymer therewith,

said polyester-urethane B being formed from a hydroxyl-bearing polyester made from at least one polyol and at least one diacid wherein

the ratio $x_{1B} = \frac{\text{Total Moles of Polyol}}{\text{Total Moles of Diacid}}$

is within the range 1.05/1-1.5/1 and the molecular weight $\bar{M}_n = 500-4,000$,

5 the ratio $x_{2B} = \frac{\text{Total Moles of Diol}}{\text{Total Moles of Polyol}}$

is within the range 5/1- ∞ ,

the ratio $x_{3B} = \frac{\text{Moles of Aromatic Acid}}{\text{Total Moles of Acid}}$

is within the range 0-0.08/1, and

10 the ratio $x_{4B} = \frac{\text{Equivalents of -NCO}}{\text{Equivalents of -OH}}$

is within the range 2/1-1.3/1.

8. An adhesive formed from:

15 A. a hydroxyl-terminated polymeric polyol having a molecular weight \bar{M}_n of about 1,000-5,000 and soluble in methyl ethyl ketone or ethyl acetate to the extent of at least 65% by weight;

20 B. an isocyanate-capped polyol-urethane having a molecular weight \bar{M}_n of about 500-4,000 and capable of forming a block copolymer with and thereby extending polyol A; and

25 C. a polyisocyanate crosslinking agent, the equivalent ratio of -OH/-NCO being about 1/1 and B supplying at least 50-94% by weight of B plus C.

9. A laminate comprising substrates 5, 7, or 8. bound together by an adhesive of any one of Claims 1 to /

30 10. In the process of forming a high solids adhesive, the steps of admixing and curing between substrates it is desired to adhere together

a polymeric polyol A having a molecular weight \bar{M}_n of about 1,000-5,000 and soluble in methyl ethyl ketone or ethyl acetate to the extent of at least 65% by weight and

an isocyanate-capped polyester-urethane
B capable of forming a block copolymer with the
polymeric polyol A,

said polyester-urethane B being formed
5 from a hydroxyl-bearing polyester made from at
least one polyol and at least one diacid wherein
the ratio $X_{1B} = \frac{\text{Total Moles of Polyol}}{\text{Total Moles of Diacid}}$
is within the range 1.05/1-1.5/1 and the molecular
10 weight $\bar{M}_n = 500-4,000$,
the ratio $X_{2B} = \frac{\text{Total Moles of Diol}}{\text{Total Moles of Polyol}}$
is within the range 5/1- ∞ ,
the ratio $X_{3B} = \frac{\text{Moles of Aromatic Acid}}{\text{Total Moles of Acid}}$
15 is within the range 0-0.8/1, and
the ratio $X_{4B} = \frac{\text{Equivalents of -NCO}}{\text{Equivalents of -OH}}$
is within the range 2/1-1.3/1.

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